
Modeling Of Catalyst Fixed Bed Reactor For Production Of

Modelling, Simulation and Optimization of
Industrial Fixed Bed Catalytic Reactors
23 European Symposium on Computer Aided
Process Engineering

Modeling of Processes and Reactors for
Upgrading of Heavy Petroleum

Multiphase Reactive Flows

Chemical Reactor Omnibook- soft cover

Multiphase Catalytic Reactors

Modelling, Simulation and Optimization of
Industrial Fixed Bed Catalytic Reactors

From the Molecular Process to the Technical
System

The Simulation of a Fixed Bed Catalytic Reactor,
in the Presence of a Rapidly Decaying Catalyst
Activation, Deactivation, and Poisoning of
Catalysts

A Computer-Aided Approach

Modeling of Catalyst Activity and Simulation of a
Hybrid Model for a Catalytic Fixed Bed Reactor

Chemical Reaction Engineering

Chemical Reactor Modeling

Modeling and Simulation of Heterogeneous
Catalytic Reactions

Catalyst Deactivation and Fixed Bed Reactor
Modeling
Modelling and Identification of a Catalytic Packed
Bed Reactor
Modeling and Simulation of Heterogeneous
Catalytic Processes
Solution of Differential Equation Models by
Polynomial Approximation
Adiabatic Fixed-Bed Reactors
Two phase, two dimensional models of fixed bed
catalytic reacto...
The Modelling and Dynamics of Catalysts and
Fixed Bed Reactors
Trickle Bed Reactors
Novel Iron Catalyst and Fixed-bed Reactor Model
for the Fischer-Tropsch Synthesis
CFD Simulation and Experiment of Catalyst
Deactivation and Heat Transfer in a Low N Fixed-
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Modeling and Simulation of Catalytic Reactors for
Petroleum Refining
Chemical Reaction Engineering
VDI Heat Atlas
Reaction Kinetics and the Development and
Operation of Catalytic Processes
Dynamic Process Modeling
Theory, Design, Manufacturing, and Applications
The Method of Volume Averaging
Fischer-Tropsch Synthesis, Catalysts, and
Catalysis
Parametric Sensitivity in Chemical Systems
Overview of the New Developments of Energy

and Petrochemical Reactor Technologies.
Projections for the 90's
Chemical and Catalytic Reactor Modeling
Chemical Reactor Design and Technology
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Practical Guides in Chemical Engineering

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**Modelling,
Simulation
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Optimization
of Industrial
Fixed Bed
Catalytic
Reactors**

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Inspired by
the leading
authority in
the field, the
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Process

Systems
Engineering at
Imperial
College

London, this
book includes
theoretical
developments,
algorithms,
methodologies
and tools in
process
systems
engineering
and
applications
from the
chemical,
energy,
molecular,
biomedical
and other
areas. It spans
a whole range
of length

scales seen in
manufacturing
industries,
from
molecular and
nanoscale
phenomena to
enterprise-
wide
optimization
and control.
As such, this
will appeal to
a broad
readership,
since the topic
applies not
only to all
technical
processes but
also due to
the
interdisciplinary
y expertise
required to

solve the challenge. The ultimate reference work for years to come.

23 European Symposium on Computer Aided Process Engineering

Walter de Gruyter GmbH & Co KG

This book provides a hybrid methodology for engineering of trickle bed reactors by integrating conventional reaction engineering models with state-of-the-art computational flow models. The content

may be used in several ways and at various stages in the engineering process: it may be used as a basic resource for making appropriate reactor engineering decisions in practice; as study material for a course on reactor design, operation, or optimization of trickle bed reactors; or in solving practical reactor engineering problems. The authors assume some background

knowledge of reactor engineering and numerical techniques. Facilitates development of high fidelity models for industrial applications Facilitates selection and application of appropriate models Guides development and application of computational models to trickle beds Modeling of Processes and Reactors for Upgrading of Heavy Petroleum Butterworth-Heinemann For more than 50 years, the

<p>Springer VDI Heat Atlas has been an indispensable working means for engineers dealing with questions of heat transfer. Featuring 50% more content, this new edition covers most fields of heat transfer in industrial and engineering applications. It presents the interrelationships between basic scientific methods, experimental techniques, model-based analysis and their transfer to technical applications.</p>	<p><u>Multiphase Reactive Flows</u> Prentice Hall With petroleum prices spiraling upward, making synthetic fuels-or "synfuels"-from coal, natural gas, and biomass has become more economically competitive. Advanced energy companies now focus exclusively on alternative fuels, and many oil companies have programs dedicated to</p>	<p>developing synthetic fuels. The Fischer-Tropsch process, which uses a <u>colle Chemical Reactor Omnibook-soft cover</u> CRC Press Abstract: Modeling of fluid flow, heat transfer and reaction in fixed beds is an essential part of their design. This is especially critical for highly endothermic reactions in low tube-to-particle diameter ratio (N) tubes, such as methane</p>
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steam reforming (MSR) and alkane dehydrogenation as two important commercial reactions. The modeling of fixed bed reaction is available in literatures with lots of assumptions. However, there is a need for implementing the reaction conditions with diffusion aspects on a real fixed bed reactor without assuming any pseudo conditions. Computational fluid dynamics

(CFD) has been found as a suitable tool by many researchers to simulate fixed beds. CFD can simulate complex geometry of randomly-packed tubes, and provides us with more fundamental understanding of the transport and reaction phenomena in reactor tubes. CFD can be used to obtain detailed three-dimensional velocity, species and temperature fields that are needed to improve engineering

approaches. Previously, the geometry of 120-degree wall segment (WS) of the whole reactor tube has been studied in our group. Previous works have introduced the coupling of gas flow and resolved species and temperature gradients inside pellets by CFD for methane steam reforming (MSR) and propane dehydrogenation (PDH) without considering deactivation. The

<p>deactivation of catalysts due to carbon formation is an important problem in industry, such as steam reforming and the catalytic dehydrogenation of alkanes, which are both strongly endothermic reactions. Many researches were carried out to study the effect of carbon formation and catalyst deactivation on the reactor performance. The local carbon deposition on catalysts can cause particle</p>	<p>breakage and strongly decrease reaction rates. Catalyst deactivation in heated tubes removes the heat sink and can result in local hot spots that weaken the reactor tube. This is particularly a problem for a low tube-to-particle diameter ratio fixed bed reactor. A 3D resolved CFD model simulation was used to study the local details of carbon deposition in which the reactions and deactivation</p>	<p>take place inside the catalytic solid particles. CFD simulations of flow, heat transfer, diffusion and reaction were carried out using the commercial CFD code FLUENT/ANSYS 6.3 in a 3D 120-degree periodic wall segment with $N=4$. The mesh used boundary layer prism cells at both the inside and outside particle surfaces and at the tube wall. These reactions were represented in the solid</p>
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particles using user-defined scalars to mimic species transport and reaction, with user-defined functions supplying reaction rates. Diffusion in the particles was modeled by Fick's law using an effective diffusivity, given by Hite and Jackson's approximation of the Dusty Gas Model. The transient developments of particle internal gradients and carbon accumulation have been studied for the early stages of

deactivation. Carbon concentration is initially strongest close to the surface and in the high temperature regions of the catalysts and affected by the wall heat flux. Deactivation of the endothermic reactions causes a slow increase in the average catalyst temperature. The second stage of the research was the verification of our CFD reaction model with experimental

data under reacting conditions. The highly endothermic commercial methane steam reforming (MSR) reaction was studied experimentally in a fixed bed reactor. The temperature contributions inside catalyst particles were measured. The MSR reaction showed strong effects on the temperature profile along the reactor. Then, a CFD model was used to predict temperature

profiles under MSR reaction conditions. Comparison of CFD and experimental data showed very good qualitative as well as quantitative agreement for temperature inside catalyst particles at different inlet gas temperatures. The last stage was to develop a fundamental energy equation without introducing new adjustable parameters to study heat transfer in fixed beds. In

the past, many researchers have been carried out to simulate the heat transfer in fixed bed reactors by using k_r (effective thermal conductivity) and h_w (heat transfer coefficient). But the classical model with k_r and h_w cannot give a correct $T(r)$ near tube wall, where deactivation is strongest. Therefore we need a better

model which can represent the near wall heat transfer more accurate. CFD modeling was used to develop pseudo-continuum model for $T(r)$ using $V_r(r, z)$ and $V_z(r)$. To get better temperature at the wall vicinity close to the physical reality. In this model radial thermal conductivity was obtained from Zehner-Schlünder model. The convection heat transfer

was calculated in the 2D flow fluid from the CFD run. Results were obtained for Reynolds numbers in the range 240-1900. The accuracy of the new model has been validated by analytical solution. The temperature calculated by the new velocity field pseudohomogeneous energy equation showed reasonable quantitative agreement with values predicted by the CFD model.

Multiphase Catalytic Reactors CRC Press Heterogeneous catalysis and mathematical modeling are essential components of the continuing search for better utilization of raw materials and energy, with reduced impact on the environment. Numerical modeling of chemical systems has progressed rapidly due to increases in computer power, and is used extensively for analysis,

design and development of catalytic reactors and processes. This book presents reviews of the state-of-the-art in modeling of heterogeneous catalytic reactors and processes. Reviews by leading authorities in the respective areas Up-to-date reviews of latest techniques in modeling of catalytic processes Mix of US and European authors, as well as academic/industrial/research

institute perspectives Connections between computation and experimental methods in some of the chapters Modelling, Simulation and Optimization of Industrial Fixed Bed Catalytic Reactors Springer Science & Business Media The Nobel Prize in Chemistry 2007 awarded to Gerhard Ertl for his groundbreaking studies in surface chemistry

highlighted the importance of heterogeneous catalysis not only for modern chemical industry but also for environmental protection. Heterogeneous catalysis is seen as one of the key technologies which could solve the challenges associated with the increasing diversification of raw materials and energy sources. It is the decisive step in most chemical industry

processes, a major method of reducing pollutant emissions from mobile sources and is present in fuel cells to produce electricity. The increasing power of computers over the last decades has led to modeling and numerical simulation becoming valuable tools in heterogeneous catalysis. This book covers many aspects, from the state-of-the-art in modeling and simulations of

heterogeneous catalytic reactions on a molecular level to heterogeneous catalytic reactions from an engineering perspective. This first book on the topic conveys expert knowledge from surface science to both chemists and engineers interested in heterogeneous catalysis. The well-known and international authors comprehensively present many aspects of the wide bridge

between surface science and catalytic technologies, including DFT calculations, reaction dynamics on surfaces, Monte Carlo simulations, heterogeneous reaction rates, reactions in porous media, electro-catalytic reactions, technical reactors, and perspectives of chemical and automobile industry on modeling heterogeneous catalysis. The result is a one-stop

reference for theoretical and physical chemists, catalysis researchers, materials scientists, chemical engineers, and chemists in industry who would like to broaden their horizon and get a substantial overview on the different aspects of modeling and simulation of heterogeneous catalytic reactions. From the Molecular Process to the Technical System CRC Press Mathematical

<p>modelling of gas-solid catalytic reactors in industry is still limited. By consolidating progress in the understanding of catalytic processes, this book applies fundamental advances to the development of models for design, simulation and optimization of industrial reactors.</p> <p><u>The Simulation of a Fixed Bed Catalytic Reactor, in the Presence of a Rapidly Decaying</u></p>	<p><u>Catalyst</u> Editions OPHRYS Reaction Kinetics and the Development and Operation of Catalytic Processes is a trendsetter. The Keynote Lectures have been authored by top scientists and cover a broad range of topics like fundamental aspects of surface chemistry, in particular dynamics and spillover, the modeling of reaction mechanisms, with special focus on the importance of</p>	<p>transient experimentation and the application of kinetics in reactor design. Fundamental and applied kinetic studies are well represented. More than half of these deal with transient kinetics, a new trend made possible by recent sophisticated experimental equipment and the awareness that transient experimentation provides more information and insight into the microphenom</p>
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ena occurring on the catalyst surface than steady state techniques. The trend is not limited to purely kinetic studies since the great majority of the papers dealing with reactors also focus on transients and even deliberate transient operation. It is to be expected that this trend will continue and amplify as the community becomes more aware of the predictive potential of fundamental kinetics when

combined with detailed realistic modeling of the reactor operation. *Activation, Deactivation, and Poisoning of Catalysts* Elsevier Inc. Chapters The continuous increase in the global demand for a cleaner energy source has instigated much interest in converting natural gas to ultra-clean fuels and value-added chemicals. Fischer-Tropsch synthesis (FTS) is a key technology for

converting syngas, produced from coal, biomass or natural gas, into a variety of hydrocarbon products. Although this technology has been around for decades, commercial development remains relatively slow and limited to use of few reactor configurations (e.g. fixed-bed reactor and slurry-bubble column reactor). On the lab-scale, supercritical solvents were utilized in FTS as a reaction

media since they have the advantages of both the gas-phase reaction (fixed-bed reactor) and the liquid-phase reaction (slurry-bubble column reactor), while simultaneously overcoming their limitations. This work focuses on modeling the behavior in the reactor bed ('macro-scale' assessment) and then zooming into the catalyst pellet itself ('micro-scale' assessment). The aim of this research

is to simulate the heat and mass transfer behavior inside the reactor bed, identify typical conditions that look at the existence and absence of both mass and heat transfer limitations, and to quantify the role of the main controlling parameters on the overall behavior of the reactor bed and on the catalyst effectiveness factor. An often used mathematical model of the fixed-bed

reactor was applied to simulate the concentration and temperature profile simultaneously based on the appropriate mass and heat balances at both scales. A second-order ordinary differential equation was used for a spherical pellet in the radial coordinate for both mass and heat balances, while a one-dimensional steady state pseudo heterogeneous model was used for the

reactor bed modeling in the axial direction. In addition, in both models the mass balance equation was expressed in terms of fugacity to account for the non-ideal behavior of the reaction mixture in the SCF-FTS. The thermodynamic properties of the mixture were estimated using the Soave-Redlich-Kwong equation of state (SRK-EOS). The simulation results of this study showed

a high temperature rise in the gas-phase FTS relative to that in the SCF-FTS under a comparable reaction conditions. Carbon monoxide conversion was considerably higher in the SCF compared to the gas-phase reaction. The effect of the particle size on the overall catalyst effectiveness factor was also investigated in both reaction media. The electronic version of this

dissertation is accessible from <http://hdl.handle.net/1969.1/151762>

A Computer-Aided

Approach

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The discovery of chaos has considerably widened the scope of our knowledge regarding the dynamics of physical systems. Gas-solid catalytic reactors are important units in the petrochemical and petroleum refining industries and in the field of

environmental protection. The knowledge required to understand and analyse the bifurcation, dynamics and chaotic behaviour of these reactors is widespread among many disciplines including chemical reaction, engineering, chemistry, physics and pure and applied mathematics. This book is the first to consolidate the progress in understanding the complex

dynamics of catalytic reactors. It covers the most important aspects of the problem, which includes the formulation of the dynamic models for these systems, the basic dynamic, bifurcation and chaotic characteristics of the different types and configurations of these units, the industrial relevance of these complex dynamic phenomena, as well as the mathematical

tools necessary for the detailed analysis of these complex dynamics. This book is easy to read, and will therefore appeal to a wide spectrum of chemical engineering students and chemical engineers in academia and in industry, also students and researchers from other disciplines who are interested in the rich and fascinating complex dynamic characteristics of gas-solid

catalytic reactors, will find it both interesting and useful.

Modeling of Catalyst Activity and Simulation of a Hybrid Model for a Catalytic Fixed Bed

John Wiley & Sons
This dissertation describes in detail the TFBRRM, reports its validation, and presents results of varying fundamental, theoretically-based parameters (e.g. effective diffusivity, Prandtl

number, friction factor, etc.) as well as physical process parameters (i.e. recycle ratio, pressure, flow rate, tube diameter, cooling temperature, and pellet diameter and shape). For example, the model predicts that decreasing effective diffusivity from $7.1E-9$ to $2.8E-9$ m²/s results in a lower maximum temperature (from 523 to 518 K) and a longer required bed

length to achieve 60% conversion of CO (from 5.7 to 8.5 m). Using the Tallmadge equation to estimate friction losses as recommended by the author results in a pressure drop 40% smaller than using the Ergun equation. Validation of the model was accomplished by matching published full-scale plant data from the SASOL Arge reactors. *Chemical Reaction Engineering* CRC Press

The Omnibook aims to present the main ideas of reactor design in a simple and direct way. It includes key formulas, brief explanations, practice exercises, problems from experience and it skims over the field touching on all sorts of reaction systems. Most important of all it tries to show the reader how to approach the problems of reactor design and what questions to ask. In effect it tries to show

that a common strategy threads its way through all reactor problems, a strategy which involves three factors: identifying the flow pattern, knowing the kinetics, and developing the proper performance equation. It is this common strategy which is the heart of Chemical Reaction Engineering and identifies it as a distinct field of study. **Chemical Reactor Modeling** Amer Chemical

Society
The worldwide petroleum industry is facing a dilemma: the production level of heavy petroleum is higher than that of light petroleum. Heavy crude oils possess high amounts of impurities (sulfur, nitrogen, metals, and asphaltenes), as well as a high yield of residue with consequent low production of valuable distillates (gasoline and diesel). These characteristics, in turn, are responsible for

the low price of heavy petroleum. Additionally, existing refineries are designed to process light crude oil, and heavy oil cannot be refined to 100 percent. One solution to this problem is the installation of plants for heavy oil upgrading before sending this raw material to a refinery. Modeling of Processes and Reactors for Upgrading of Heavy Petroleum gives an up-to-date treatment of

modeling of reactors employed in the main processes for heavy petroleum upgrading. The book includes fundamental aspects such as thermodynamics, reaction kinetics, chemistry, and process variables. Process schemes for each process are discussed in detail. The author thoroughly describes the development of correlations, reactor models, and

kinetic models with the aid of experimental data collected from different reaction scales. The validation of modeling results is performed by comparison with experimental and commercial data taken from the literature or generated in various laboratory scale reactors. Organized into three sections, this book deals with general aspects of properties and upgrading of heavy oils,

describes the modeling of non-catalytic processes, as well as the modeling of catalytic processes. Each chapter provides detailed experimental data, explanations of how to determine model parameters, and comparisons with reactor model predictions for different situations, so that readers can adapt their own computer programs. The book includes rigorous

treatment of the different topics as well as the step-by-step description of model formulation and application. It is not only an indispensable reference for professionals working in the development of reactor models for the petroleum industry, but also a textbook for full courses in chemical reaction engineering. The author would like to express his sincere appreciation to the Marcos

Moshinsky Foundation for the financial support provided by means of a Cátedra de Investigación.
Modeling and Simulation of Heterogeneous Catalytic Reactions
Bruce Alan Finlayson
This book illustrates how models of chemical reactors are built up in a systematic manner, step by step. The authors also outline how the numerical solution algorithms for reactor

models are selected, as well as how computer codes are written for numerical performance, with a focus on MATLAB and Fortran. Examples solved in MATLAB and simulations performed in Fortran are included for demonstration purposes.

Catalyst Deactivation and Fixed Bed Reactor

Modeling
Walter de Gruyter GmbH & Co KG
Catalytic Reactors presents several key

aspects of reactor design in Chemical and Process Engineering. Starting with the fundamental science across a broad interdisciplinary field, this graduate level textbook offers a concise overview on reactor and process design for students, scientists and practitioners new to the field. This book aims to collate into a comprehensive and well-informed work of leading researchers

from north America, western Europe and south-east Asia. The editor and international experts discuss state-of-the-art applications of multifunctional reactors, biocatalytic membrane reactors, micro-flow reactors, industrial catalytic reactors, micro trickle bed reactors and multiphase catalytic reactors. The use of catalytic reactor technology is

essential for the economic viability of the chemical manufacturing industry. The importance of Chemical and Process Engineering and efficient design of reactors are another focus of the book. Especially the combination of advantages from both catalysis and chemical reaction technology for optimization and intensification as essential factors in the future development of reactors and processes

are discussed. Furthermore, options that can drastically influence reaction processes, e.g. choice of catalysts, alternative reaction pathways, mass and heat transfer effects, flow regimes and inherent design of catalytic reactors are reviewed in detail. Focuses on the state-of-the-art applications of catalytic reactors and optimization in the design and operation of industrial

catalytic reactors
Insights into transfer of knowledge from laboratory science to industry For students and researchers in Chemical and Mechanical Engineering, Chemistry, Industrial Catalysis and practising Engineers
Modelling and Identification of a Catalytic Packed Bed Reactor
Elsevier
Provides a holistic approach to multiphase catalytic

reactors from their modeling and design to their applications in industrial manufacturing of chemicals Covers theoretical aspects and examples of fixed-bed, fluidized-bed, trickle-bed, slurry, monolith and microchannel reactors Includes chapters covering experimental techniques and practical guidelines for lab-scale testing of multiphase reactors Includes mathematical

content focused on design equations and empirical relationships characterizing different multiphase reactor types together with an assortment of computational tools Involves detailed coverage of multiphase reactor applications such as Fischer-Tropsch synthesis, fuel processing for fuel cells, hydrotreating of oil fractions and biofuels processing *Modeling and Simulation of*

Heterogeneous Catalytic Processes Cambridge University Press Practical Guides in Chemical Engineering are a cluster of short texts that each provides a focused introductory view on a single subject. The full library spans the main topics in the chemical process industries that engineering professionals require a basic understanding of. They are 'pocket publications' that

professional engineers can easily carry with them or access electronically while working. Each text is highly practical and applied, and presents first principles for engineers who need to get up to speed in a new area fast. The focused facts provided in each guide will help you converse with experts in the field, attempt your own troubleshooting, check calculations, and solve rudimentary problems.

Adiabatic Fixed-bed Reactors covers the fundamentals of fixed-bed reactors, including various types and their physical properties. Applications of each device type are discussed, as well as trouble-shooting Solid-supported Catalysts. This text is ideal for any engineer who is new to working with fixed-bed reactors and needs to know the basics quickly and easily.

Practical, short, concise information on the basics will help you get an answer or teach yourself a new topic quickly. Supported by industry examples to help you solve a real world problem. Single subject volumes provide key facts for professionals. *Solution of Differential Equation Models by Polynomial Approximation* Elsevier. The behavior of a chemical system is affected by many

physicochemical parameters. The sensitivity of the system's behavior to changes in parameters is known as parametric sensitivity. When a system operates in a parametrically sensitive region, its performance becomes unreliable and changes sharply with small variations in parameters. Thus, it is of great value to those who design and operate chemical systems to be

able to analyze and predict their sensitivity behavior. This book is the first to provide a thorough treatment of the concept of parametric sensitivity and the mathematical tool it generated, sensitivity analysis. The emphasis is on applications to real situations. The book begins with definitions of various sensitivity indices and describes the numerical techniques most

commonly used for their evaluation. Extensively illustrated chapters discuss sensitivity analysis in a variety of chemical reactors--batch, tubular, continuous-flow, fixed-bed--and in combustion systems, mechanistic studies, air pollution, and metabolic processes. Seniors and graduate students in various fields of science and engineering, researchers, and practicing engineers will

welcome this valuable resource. John Wiley & Sons Today's frustrations and anxieties resulting from two energy crises in only one decade, show us the problems and fragility of a world built on high energy consumption, accustomed to the use of cheap non-renewable energy and to the acceptance of existing imbalances between the resources and demands of countries. Despite all

these stressing factors, our world is still hesitating about the urgency of undertaking new and decisive research that could stabilize our future, Could this trend change in the near future? In our view, two different scenarios are possible. A renewed energy tension could take place with an unpredictable timing mostly related to political and economic factors, This

could bring again scientists and technologists to a new state of shock and awaken our talents, A second interesting and beneficial scenario could result from the positive influence of a new generation of researchers that with or without immediate crisis, acting both in industry and academia, will face the challenge of developing technologies and processes to pave the way to a less

vulnerable
society,
Because
Chemical
Reactor
Design and
Technology
activities are

at the heart of
these required
new
technologies
the timeliness
of the NATO-
Advanced

Study Institute
at the
University of
Western
Ontario,
London, was
very
appropriate.